Stokes's theorem

Suppose S is an oriented suface in \mathbb{R}^3 (means that there is a continuously varying unit normal at all points of S) Which is well behaved and bounded by a closed curve C (or possibly a finite number of closed curves) and suppose C is oriented so that S is to the left. Let $\mathbf{F} = \mathbf{F}(x, y, z) = [F_1, F_2, F_3]$ be a vector field well-behaved on S and its boundary C. Then

$$\iint_{S} (\nabla \times \mathbf{F}) \cdot \mathbf{n} \, dA = \oint_{C} \mathbf{F} \cdot d\mathbf{x}$$

Examples. (i) Green's theorem (S planar). (ii) S a closed surface like a sphere (no C).

Green's theorem

Another way to write the theorem (equivalant way) is: Assume $\mathbf{F}(x, y) = [F_1(x, y), F_2(x, y)]$ is well behaved in a region of the plane that includes an anticlockwise simple closed curve *C* and its interior *R*. Suppose n is the unit normal to *C* pointing outwards. Then

$$\oint_C \mathbf{F} \cdot \mathbf{n} \, ds = \iint_R \nabla \cdot \mathbf{F} \, dx \, dy$$

(ds = arclength).

Reason. $\mathbf{T} = \frac{dx}{ds}\mathbf{i} + \frac{dy}{ds}\mathbf{j}$ is the unit tangent vector to *C*. $\mathbf{n} = \frac{dy}{ds}\mathbf{i} - \frac{dx}{ds}\mathbf{j}$. Hence $\mathbf{F} \cdot \mathbf{n} \, ds = F_1 \, dy - F_2 \, dx$.

Heat equation

We consider a heated solid object. u(x, y, z, t) =temperature at position (x, y, z) and at time t.

Law of heat flow: Heat will flow in direction of maximum decrease of termperature, that is in the direction of $-\nabla u = -[\frac{\partial u}{\partial x}, \frac{\partial u}{\partial y}, \frac{\partial u}{\partial z}]$ at a rate proportional to $\|\nabla u\|$. Flow rate $= K \|\nabla u\|$ with K = thermal conductivity.

We assume K > 0 constant. Consider any subregion

R inside the solid with boundary surface S.

 $\iint_{S} -K(\nabla u) \cdot \mathbf{n} \, dS = \text{rate of heat flow out of } S.$ (Pictorially $(\nabla u) \cdot \mathbf{n} \, dS = \|\nabla u\| \cos \theta \, dS = \|\nabla u\|$ area of infinitesimal section dS times cosine of angle with direction of flow (effective cross sectional area for flow from dS).

On the other hand, total heat inside *R* at any time is $\iiint_R \sigma \rho u \, dx \, dy \, dz$ (with σ = specific heat, ρ = density of material). Computing rate of decrease of heat (or

rate of heat loss) in two ways

$$\iint_{S} -K(\nabla u).\mathbf{n} \, dS = -\frac{\partial}{\partial t} \iiint_{R} \sigma \rho u \, dx \, dy \, dz$$

Apply Gauss' theorem on the left and bring the deriviative inside the integral on the right

$$\iint_{R} -K \operatorname{div} (\nabla u) \, dx \, dy \, dz = \iint_{R} -\sigma \rho \frac{\partial u}{\partial t} \, dx \, dy \, dz$$
$$\iint_{R} (\sigma \rho \frac{\partial u}{\partial t} - K \nabla^{2} u) \, dx \, dy \, dz = 0$$

True for all small regions R inside solid. Forces

$$\frac{\partial u}{\partial t} = \frac{K}{\sigma \rho} \nabla^2 u$$

$$\frac{\partial u}{\partial t} = c^2 \nabla^2 u$$

with $c^2 = K/(\sigma \rho)$ = thermal diffusivity of the material.

Remark. If the heat distribution is in a steady state (*i.e.* no t dependence in u) then $\partial u/\partial t = 0$. Hence $\nabla^2 u = 0$ (u satisfies Laplace's equation).

Remark. To derive the Heat equation for 2-dimensions (no z) can either use 2-D version of the divergence theorem (= version of Green's theorem stated after Stokes' above) or just assume u(x, y, z, t)independent of z. **Remark.** For 1-dimensional heat equation, can either use latter aproach (assume no y or z dependence) or look at thin rod with temperature u(x,t) and heat flow proprtional to $-\partial u/\partial x$. Instead of Gauss' theorem use

$$\int_{\alpha}^{\beta} \frac{\partial^2 u}{\partial x^2} dx = \frac{\partial u}{\partial x} (\beta, t) - \frac{\partial u}{\partial x} (\alpha, t)$$

Exercise: Try to work this argument through.